

## COMMUNICATION

ALBERTO ROZZI\*, ALBERTO BRUNETTI\*

## ANAEROBIC PROCESS CONTROL BY INORGANIC CARBON ANALYSIS

## 1. INTRODUCTION

Stability in the anaerobic treatment of sludges and of industrial wastewaters is closely related to the buffering action of  $\text{CO}_2/\text{HCO}_3^-$  and to the total volatile acids concentration (TVA) and requires the monitoring of the following parameters:  $\text{H}^+$ , TVA, total alkalinity (TA) and bicarbonate ( $\text{HCO}_3^-$ ) concentrations in the digester mixed liquor and  $\text{CO}_2/\text{CH}_4$  ratio in the gas [1, 4-7].

Routine process analysis is based on TA and TVA titrations and  $\text{HCO}_3^-$  determination (eq. (1)). As well known, TVA analysis [2] is time consuming and not very accurate.

In this note a simple procedure for the calculation of  $\text{HCO}_3^-$  alkalinity in digester mixed liquors, based on an inorganic carbon mass balance, is presented.

## 2. METHODS AND MATERIALS

Neglecting weak anions, such as phosphates and silicates, the alkalinity balance gives bicarbonate concentration in a water solution:

$$\text{HCO}_3^- = \text{TA} - 0.833 \cdot (1-a) \cdot \text{TVA}, \quad (1)$$

where:

$\text{HCO}_3^-$  — bicarbonate concentration as  $\text{CaCO}_3$ ;

TA — total alkalinity concentration as  $\text{CaCO}_3$ ;

TVA — total volatile acids concentration as  $\text{CH}_3\text{COOH}$ ;

0.833 — equivalent weights ratio  $\text{CaCO}_3/\text{CH}_3\text{COOH}$ ;

$a$  — fraction of ionized acid in solution at the final titration pH (for  $\text{CH}_3\text{COOH}$  and pH

= 3.7,  $a = 0.08$ ).

Bicarbonates can also be determined from an inorganic carbon (IC) balance in solution:

$$\text{IC} = \text{CO}_2 + \text{HCO}_3^- + \text{CO}_3^{2-}. \quad (2)$$

\* Institute di Ricerca sulle Acque del C.N.R., Via F. de Blasio 5, 70123 Bari, Italy.

If  $\text{pH} \leq 8$  (as in anaerobic digesters) then  $\text{CO}_3^{--}$  is negligible:

$$\text{CO}_3^{--} \leq 6 \cdot 10^{-3} \cdot \text{IC} \quad (\text{T} = 37^\circ\text{C})$$

and eq. (2) is reduced to:

$$\text{HCO}_3^- = \text{IC} - \text{CO}_2.$$

The following quick and easy method for determining the  $\text{HCO}_3^-$  concentration in digester mixed liquors has been adopted:

1. Calculation of concentration of  $\text{CO}_2$  in mixed liquor as a function of partial pressure of  $\text{CO}_2$  gas, according to Henry law (assuming equilibrium conditions at the gas/liquid interfaces).
2. Determination of inorganic carbon concentration in the mixed liquor.
3. Determination of TA by strong acid/weak base titration.
4. Calculation of  $\text{HCO}_3^-$  concentration by eq. (4) and of TVA concentration by eq. (1).

The method was tested on mixed liquor and gas samples from laboratory and pilot plant ( $5 \text{ dm}^3$  and  $2 \text{ m}^3$ , respectively) digesters fed with olive oil mill wastewaters ( $\text{TOC} = 15,000$  to  $30,000 \text{ mg/dm}^3$ ;  $\text{CO}_2 = 35,000$  to  $70,000 \text{ mg O}_2/\text{dm}^3$ ;  $K = 3,000$  to  $6,000 \text{ mg/dm}^3$ ).

Concentrations of gaseous  $\text{CO}_2$  were determined by injecting gas samples into the inorganic chamber of a Beckman, Fullerton, Mod. 915 Total Organic Carbon Analyser, using pure  $\text{CO}_2$  as reference [1].

Concentration of  $\text{CO}_2$  in mixed liquor was calculated assuming Henry constant  $H_{37^\circ\text{C}} = 2211 \text{ bar} \cdot \text{mole/mole}$ .

Inorganic carbon concentration in mixed liquor was determined by using the same TOC analyser. Because of the significance of IC determinations, stripping of  $\text{CO}_2$  from the samples was carefully avoided.

Total alkalinity was determined by potentiometric titration using  $0.02\text{N H}_2\text{SO}_4$  in a radiometer Copenhagen, ABU 12 Autoburette.

### 3. RESULTS AND DISCUSSION

Concentrations of  $\text{HCO}_3^-$ , determined by the proposed IC method ( $\text{BA}_1$ ) and by traditional TA/TVA procedure ( $\text{BA}_2$ ), are for comparative reasons given in the table. The values obtained by the IC method are always lower than those obtained by TA/TVA method ( $7 \div 14\%$ ); these differences are explained in the following way:

IC errors:  $\text{BA}_1$  values are affected by errors in IC and  $\text{CO}_2$  determinations. IC instrumental errors on 915 TOC Analyser are of order of 1%; errors due to a lack of balance between liquid/gas interface and/or those due to evaluation of Henry constant are difficult to estimate; nevertheless the influence should be weak ( $\approx 1.5\%$ ), as in ordinary digester conditions  $\text{CO}_2 \leq 0.15 \cdot \text{IC}$ , and a 10% error in determination of  $[\text{CO}_2]$  does not seem possible; hence reliable  $\text{HCO}_3^-$  measurements can be obtained by the IC method and the accuracy depends mainly on the instrumentation performance.

TA/TVA errors:  $\text{BA}_2$  values are considerably affected by the following analytical errors: 1. TA titration takes also account of the contribution of the weak anions such as phosphates, silicates etc.; 2. TVA chromatographic analysis does not allow a complete extraction of the organic acids (recovery  $\geq 95\%$ ). Consequently,  $\text{BA}_2$  values determined by TA/TVA procedure are surely overestimated.

TVA determination making use of  $\text{HCO}_3^-$  (by IC method and TA titration) is not accurate (overestimated values are obtained) because alkalinity related to  $\text{PO}_4^-$  etc. (which in the traditional method affects the  $\text{HCO}_3^-$  value) is now "transferred" completely on TVA (eq. (1)).

In order to obtain more reliable TVA values by the IC method, a correction factor  $\Delta\text{TA}$  excluding the influence of the interfering weak anions can be calculated as follows:

$$\Delta\text{TA} = \text{TA} - \text{BA}_1 - \text{TVA}, \quad (5)$$

where TVA is determined by an independent method on few samples only.

Table

HCO<sub>3</sub><sup>-</sup> determinations by TVA/TA and by proposed IC methods  
 Oznaczenie HCO<sub>3</sub><sup>-</sup> za pomocą metody TVA/TA oraz proponowanej metody IC

IC mg/dm <sup>3</sup> C	CO <sub>2</sub> (gas) %	CO <sub>2</sub> (sol.) mg/dm <sup>3</sup> C	(HCO <sub>3</sub> <sup>-</sup> ) <sub>1</sub> mg/dm <sup>3</sup> CaCO <sub>3</sub>	TA mg/dm <sup>3</sup> CaCO <sub>3</sub>	TVA mg/dm <sup>3</sup> HAc	pH	(HCO <sub>3</sub> <sup>-</sup> ) <sub>2</sub> mg/dm <sup>3</sup> CaCO <sub>3</sub>	$\frac{\Delta(\text{HCO}_3^-)}{(\text{HCO}_3^-)_2}$ %
898	39.8	117	3252	4270	849	7.07	3620	10.2
805	39.0	115	2875	3937	765	7.00	3351	14.2
173	25.8	76	402	925	610	6.39	468	14.1
790	35.0	103	2863	4440	1758	7.05	3093	7.4
900	36.0	106	3308	4700	1289	7.06	3712	10.9
1120	42.0	124	4150	6820	3000	7.05	4521	8.2

CO<sub>2</sub> Henry constant H<sub>37°C</sub> = 2211 bar

The above procedure implies constant concentration of interfering weak anions, which is a reasonable assumption for digester in steady-state operation. This correction is not really necessary because, in anaerobic process monitoring, the variations of control parameters are more important than the absolute values.

In conclusion, the inorganic carbon procedure for determining  $\text{HCO}_3^-$  concentration is a quick and reliable method for anaerobic process monitoring which could easily be automated by TA and IC (mixed liquor and gas) instrumental analyses.

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